

# Burnout Correlations for Even - and Odd-Numbered Peripheral Rod Clusters over Low Pressure Range

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## ABSTRACT

Burnout data with low pressure Freon-113 for even- and odd- numbered peripheral rod clusters with relatively large spacings were used to derive equations in terms of dimensionless parameters suggested by Barnett. The equations which are for three different flow regimes for each rod geometry (even or odd) were found to predict burnout data with maximum RMS deviation being 3.8%.

## INTRODUCTION

For large rod spacings, burnout data and correlations are practically nonexistent. Based on experiments in a simpler annular geometry, Bernath [1] derived a set equations which sometimes applied to rod bundles with large spacings but it is still not clear if these equations are applicable for the latter case.

In a preceding study Berger and Akaho [2] reported burnout results for Freon-113 obtained in a low pressure range of 101.3 - 165kPa ( $\rho/\rho_s = 205 - 113$ ) for even- and odd-numbered peripheral rod clusters as illustrated in Figure 1. The rods with a diameter of 4.76mm were uniformly spaced in the free flow area. The geometrical characteristics of the tested clusters are listed in Table 1. The spacings are relatively large, 3.14 - 11.03mm. Significant differences in the behaviour of burnout conditions were noticed for evens and odds. These observations are found to be consistent with those made by Macbeth [3]. For each geometry, three flow regimes called A-(burnout of dryout type), C-(burnout in nucleate boiling) and B-(intermediate between A and C) were identified, which is consistent with earlier investigations of Katto [4] and Dukler [5].

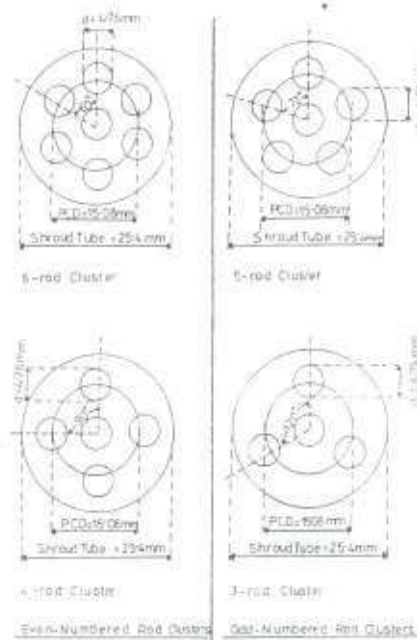


Fig. 1: Cross-section of Rod Bundles with Unheated Central Rods.

Apart from the C-region for even-numbered clusters the burnout data followed the single linear  $\phi_b - \Delta H_f$  relationship as discussed for instance in Collier's book [6]. In the C-region for evens there occurred a change of slope of the  $\phi_b - \Delta H_f$  lines as also noticed by Kirby et al [7] with low pressure water in annular geometry.

The exit quality,  $\chi_{ex}$ , for a given  $\Delta H_f$  and mass flow rate  $m$  was determined from the energy balance on the test section as:

$$\chi_{ex} = \left[ \frac{Q_b}{\dot{m} H_{fg}} \right] - \left[ \frac{\Delta H_f}{H_{fg}} \right] \quad (1)$$



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**Table 1: Characteristics of Tested Clusters.**

	Units	Rod Cluster			
		6	5	4	3
FCD x 10 <sup>3</sup>	m	15.08	15.08	15.08	15.08
A <sub>w</sub> x 10 <sup>3</sup>	m	382.14	399.78	418.00	435.58
P <sub>1</sub> x 10 <sup>3</sup>	m	89.72	74.78	59.82	44.86
A <sub>v</sub> x 10 <sup>3</sup>	m	44.86	37.39	29.91	22.42
α <sub>s</sub>	%	28.15	22.96	18.19	13.84
d <sub>1</sub> x 10 <sup>3</sup>	m	17.04	21.38	27.95	38.84
d <sub>2</sub> x 10 <sup>3</sup>	m	14.61	17.82	22.36	29.13
l <sub>1</sub> /d <sub>1</sub>	-	29.35	23.38	17.89	12.87
p/d	-	1.66	1.99	2.49	3.82

The variation of burnout in the low pressure range was found to follow an exponential relationship of the simple form:

$$\frac{\phi_b}{\phi_{b1}} = \left[ \frac{P}{P_1} \right]^\alpha \quad (2)$$

where α is different for the various flow regimes but of equal value if the geometry of rod cluster (even or rod) is the same.

In this report the burnout data are correlated in terms of dimensionless parameters that can be found in the scaling laws derived by Barnett [8]. The method of analysis with the simplifying assumptions which made the derivation of equations possible is explained. The boundaries between the flow regimes are established. Also, discussed is the criterion for determining the exit quality at which a break will occur in the burnout-exit quality relationship in the C-regime. The equations derived from experiments with Freon-113 burnout data were used to predict water data and the possibility of applying them to other saturated liquids was considered.

**2. CORRELATING EQUATIONS**

Barnett [8] suggested the following relationship for burnout in saturated flows:

$$\frac{\phi_b^2 x^{1/2}}{H_{fg} \rho_1^{1/2}} = f \left( \frac{G \gamma^{1/2}}{\rho_1^{1/2} P_1}, \frac{P_1}{P_v}, \frac{\Delta H_f}{2h_{fg}}, \frac{\lambda_b}{d_b}, \frac{Q_{w-p} \rho_1^{1/2}}{\lambda_b} \right) \quad (3)$$

The dimensionless parameters should permit the modelling of burnout results from one saturated fluid to another, e.g. from Freon-113 to water.

They were later found to be suitable also for scaling burnout fluxes in subcooled Freon-113 [9]. To adapt the expression for the present case the following assumptions were made:

(a) The last dimensionless group was neglected since, in the tested range of pressure, the variations of cp and k<sub>s</sub> were small and the other terms appear in the remaining groups. This is also consistent with the findings of Jones and Hoffman [10] and of Aladevov et al [11] that cp and k<sub>s</sub> are unimportant and have no effect on φ<sub>b</sub>.

(b) It was earlier stated that the φ<sub>b</sub> values follow a linear relationship with ΔH<sub>f</sub>. Therefore we can write

$$\phi_b = \phi_b^* + K \frac{\Delta H_f}{H_{fg}} \quad (4)$$

which can be expressed in the form

$$\delta_b = \phi_b^* \left( 1 + K \frac{\Delta H_f}{H_{fg}} \right) \quad (5)$$

where K = κ/φ<sub>b</sub><sup>\*</sup> and φ<sub>b</sub><sup>\*</sup> is the burnout flux at zero subcooling (ΔH<sub>f</sub>=0) which can be correlated in the form:

$$\frac{\phi_b^* x^{1/2}}{H_{fg} \rho_1^{1/2}} = f \left( \frac{G \gamma^{1/2} P}{\rho_1^{1/2} P_1}, \frac{P_1}{P_v}, \frac{\lambda_b}{d_b} \right) \quad (6)$$

The term Gγ<sup>1/2</sup>/ρ<sub>1</sub><sup>1/2</sup> from Eqn. (3) was modified to Gγ<sup>1/2</sup>p/ρ<sub>1</sub><sup>1/2</sup>p<sub>1</sub> because it was found that Gγ<sup>1/2</sup>p/ρ<sub>1</sub><sup>1/2</sup>p<sub>1</sub> remains fairly constant for a particular coolant within the test pressure range i.e. for Freon-113 in the range of 101.3 - 165kPa. This applies to other coolants i.e. H<sub>2</sub>O, Freon-112, NH<sub>3</sub> and Hg for

density ratio in the range  $\rho_1/\rho_v = 205 - 125$ . Thus, it becomes possible to vary the parameter  $G_1^2 \rho_1^{1/2} / \rho_v^{1/2}$  while  $\rho_1/\rho_v$  (pressure dependent) and  $l_b/d_b$  were kept constant.

(c) The number of  $l_b/d_b$  ratio in the tested clusters was limited to two for each of the rod configurations (even or odd). Therefore, it had to be assumed that the dependence on  $l_b/d_b$  was hyperbolic as found by earlier researchers [4, 12].

Consequently,

$$\phi_b^n = f \left[ \frac{1}{a + b(l_b/d_b)} \right] \quad (7)$$

The  $\phi_b^n$  term appearing on the RHS of Eqn. (5) can be correlated in terms of the parameters suggested in Eqn. (6) which is finally expressed as:

$$\frac{\phi_b^n G_1^{1/2} \rho_1^{1/2}}{H_{LH} \rho_1^{1/2}} = \frac{f \left[ \frac{G_1^{1/2} \rho_1^{1/2}}{\rho_v^{1/2} \rho_1} \right] \times f \left[ \frac{l_b}{d_b} \right]}{f \left[ \frac{\rho_1}{\rho_v} \right]} \quad (8)$$

The  $\phi_b^n$  data were obtained from the intersects of the  $\phi_b \Delta H_i$  lines with the  $\phi_b$  - axis. In view of the difficulties in maintaining  $\Delta H_i = 0$ , the extrapolated values were used instead of direct measurements. The  $\phi_b^n$  data expressed in the dimensionless form as on the LHS of Eqn. (6) was plotted against  $G_1^2 \rho_1^{1/2} / \rho_v^{1/2}$  for fixed  $\rho_1/\rho_v$  (and hence fixed pressure) and for a given cluster yielded a curve with different slopes in the flow regimes. The graphical representation of the  $\phi_b^n$  data for the 6-rod (even) and 5-rod are presented in Figs. 2 and 3 respectively. It was for each cluster geometry according to Eqn. (6).

The form of Eqn.(5) is valid in all flow regimes except for the even-clusters in the C-regime which is characterised by high flow rates. Here, the dependence of  $\phi_b$  on  $(\Delta H_i/H_{LH})$  is represented by straight lines with different slopes called  $K_L$  and  $K_H$ . The subscripts L and H denote low and high enthalpies respectively. In the H-regime a factor  $\beta$  was required to account for the change of slope of the  $\phi_b - \Delta H_i$  line. Eqn. (5) is then modified to

$$\phi_b = \beta \phi_b^n \left[ 1 + K_H \frac{\Delta H_i}{H_{LH}} \right] \quad (9)$$

The slope K in Eqns. (5) and (9) could be determined by choosing an arbitrary value of  $(\Delta H_i)_a$  and expressing the corresponding burnout fluxes  $\phi_b^{na}$  found on the  $\phi_b - \Delta H_i$  line in terms of the parameters in Eqn.(6).

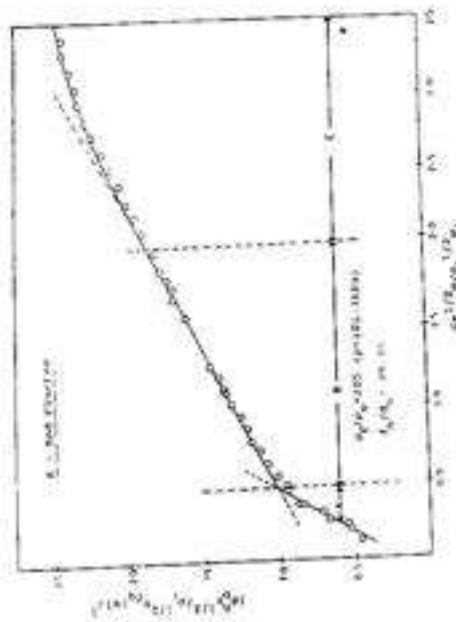


Fig. 2: Graphical Representation of 6-rod Cluster  $\phi_b^n$  Data A-, B- and C-Regimes.

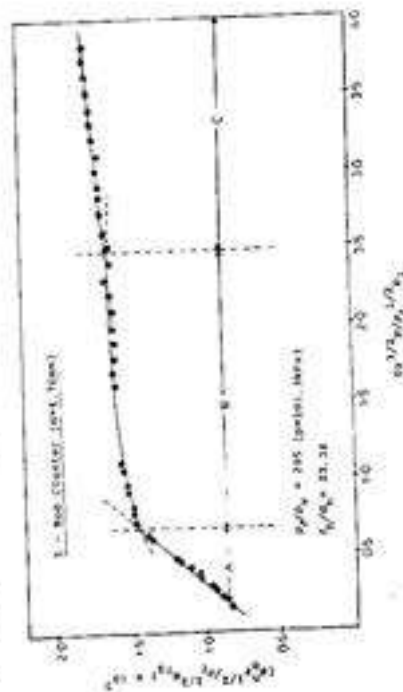


Fig. 3: Graphical Representation of 5-rod Cluster  $\phi_b^n$  Data A-, B- and C-Regimes.

Since  $\phi_{b1}^*$  is related to  $\phi_{b1}^0$  by Eqn.(5) or (9) as:

$$\phi_{b1}^* = \phi_{b1}^0 \left( 1 + K_p \frac{(\Delta H_d)_m}{H_{fg,p}} \right) \quad (10)$$

the slope  $K_p$  becomes

$$K_p = \frac{H_{fg,p}}{(\Delta H_d)_m} \left( \frac{\phi_{b1}^*}{\phi_{b1}^0} - 1 \right) \quad (11)$$

$\phi_{b1}^*$  was correlated in the same way as  $\phi_{b1}^0$  in terms of the dimensionless parameters. Representing the slope at any pressure as  $K_p$  with  $H_{fg}$  as  $(H_{fg})_p$  then Eqn. (11) can be rewritten using the correlated forms:

$$K_p = \frac{(H_{fg})_p}{(\Delta H_d)_m} \left[ f_p^* \left( \frac{G_p^{1/2} D_p}{\rho_p^{1/2} D_p}, \frac{l_h}{D_p}, \frac{l_h}{D_p} \right) / \left[ f_p^* \left( \frac{G_p^{1/2} D_p}{\rho_p^{1/2} D_p}, \frac{l_h}{D_p}, \frac{l_h}{D_p} \right) - 1 \right] \right] \quad (12)$$

Using the experimental result presented in Eqn.(2),  $\phi_{b1}^*$  and  $\phi_{b1}^0$  can be related to the values at 1 bar,  $\phi_{b1}^{*1}$  and  $\phi_{b1}^{01}$  respectively as:

$$\phi_{b1}^* = \phi_{b1}^{*1} \left( \frac{p}{p_1} \right)^\alpha \text{ and } \phi_{b1}^0 = \phi_{b1}^{01} \left( \frac{p}{p_1} \right)^\alpha \quad (13)$$

Substituting for  $\phi_{b1}^*$  and  $\phi_{b1}^0$  in Eqn. (10) using the expressions (13) gives the expression

$$\phi_{b1}^{*1} \left( \frac{p}{p_1} \right)^\alpha = \phi_{b1}^{01} \left( \frac{p}{p_1} \right)^\alpha \left( 1 + K_p \frac{(\Delta H_d)_m}{(H_{fg})_p} \right) \quad (14)$$

The above equation is valid for any pressure greater than 1 bar, and for 1 bar conditions, it simplifies to the form

$$\phi_{b1}^{*1} = \phi_{b1}^{01} \left( 1 + K_1 \frac{(\Delta H_d)_m}{(H_{fg})_1} \right) \quad (15)$$

Now dividing Eqn.(14) by Eqn.(15), shows that

$$\frac{K_p / (H_{fg})_p}{K_1 / (H_{fg})_1} = \frac{\left( \frac{\phi_{b1}^*}{\phi_{b1}^0} / \frac{\phi_{b1}^{*1}}{\phi_{b1}^{01}} \right)^\alpha - 1}{\left( \frac{\phi_{b1}^*}{\phi_{b1}^0} / \phi_{b1}^{01} \right)^\alpha - 1} = 1 \quad (16)$$

for a specified cluster geometry in a flow regime where  $\alpha$  value remains the same. Thus, the change of  $K$  with pressure is given by

$$K_p = \left( \frac{(H_{fg})_p}{(H_{fg})_1} \right) K_1 \quad (17)$$

Eqn.(12) can be modified using fluid properties of Freon-113 at 1 bar [ $\rho_l/\rho_v = 205$ ,  $(H_{fg})_1 = 145.9 \text{ kJ/kg}$ ] to determine an expression for  $K_1$ ; leading to

$$K_1 = \frac{(H_{fg})_1}{(\Delta H_d)_m} \left\{ \left[ f_1^* \left( \frac{G_1^{1/2}}{\rho_1^{1/2}}, \frac{l_h}{D_h} \right) / \left[ f_1^* \left( \frac{G_1^{1/2}}{\rho_1^{1/2}}, \frac{l_h}{D_h} \right) - 1 \right] \right] \right\} \quad (18)$$

Now, it is possible to determine  $K_p$  (the slope of  $\phi_{b1} - \Delta H_d$  line for any pressure greater than 1 bar) by relating it to  $K_1$  calculated from Eqn.(18) using expression (17).

In the limited pressure range of the present experiments (101.3 - 165kPa) the variation of  $H_{fg}$  is small and therefore,  $\kappa$  in Eqn.(4) is strongly dependent on pressure. Normalizing  $\kappa$  and  $\phi_{b1}^*$  yields a coefficient  $K$  which is virtually independent of pressure, at least in the tested range.

#### (i) Expression for $\phi_{b1}^*$

Two forms of expressions were derived for predicting the values. One form is applicable to data in those flow regimes where  $\phi_{b1}^* \gamma_w / \rho_l H_{fg}$  vs.  $G_p^{1/2} p / \rho_l^{1/2} p_1$  followed a linear relationship for fixed  $\rho_l/\rho_v$  and  $\gamma_w/\rho_l$ . The other form of equation is valid for regimes where the variation with  $G_p^{1/2} p / \rho_l^{1/2} p_1$  was exponential. It was found out that the variation with  $\rho_l/\rho_v$  was exponential and it was stated earlier that the variation with  $l_h/d_s$  was assumed to be hyperbolic. Thus the explicit form of Eqn.(6) is either

$$\frac{\phi_{b1}^{*1/2}}{H_{fg}^{1/2} p_1^{1/2}} = c_1 \left[ 1 + c_2 \left( \frac{G_p^{1/2} p}{\rho_l^{1/2} p_1} \right) \right] \left[ 1 + c_3 \frac{l_h}{d_s} \right] \left( \frac{p_l}{p_v} \right)^\alpha \quad (19)$$

or

$$\frac{\phi_{b1}^{*1/2}}{H_{fg}^{1/2} p_1^{1/2}} = c_1 \left[ \frac{G_p^{1/2} p}{\rho_l^{1/2} p_1} \right]^\alpha \left[ 1 + c_2 \frac{l_h}{d_s} \right] \left( \frac{p_l}{p_v} \right)^\alpha \quad (20)$$

Eqn.(19) applies to data in flow regimes A and B of even clusters to A and C of the odd-clusters. In flow regime C of even-geometry and B of odd configuration Eqn.(20) is applicable.

Different numerical values of the exponents and coefficients have been obtained for the even- and odd-numbered clusters in each of the three flow regimes. A list of them is provided in Table 2.

In order to determine the parameter  $\beta$  associated with Eqn.(9) when burnout values are within H-(high enthalpy) regime for the C-regime of even-numbered clusters, another burnout value called  $\phi_b^*$  was obtained at the intersect of the H-regime line

Table 2(a) Constants and Exponents of Eqn. (19)

Geometry	Flow Regime	$c_1 \times 10^4$	$c_2$	$c_3 \times 10^3$	
Even	A	8.96	7.416	1.50	-0.263
	B	17.40	0.857	14.40	-0.112
Odd	A	32.75	2.129	57.60	-0.161
	C	382.50	0.073	7.60	-0.593

Table 2(b) Constants and Exponents of Eqn.(20)

Geometry	Flow Regime	$k_1 \times 10^3$	$k_2 \times 10^3$	$\nu$	
Even	C	2.961	3.60	0.402	-0.110
Odd	B	36.350	7.80	0.080	-0.566

### (ii) Expressions for K

Expressions for determining the parameter K (a measure of steepness of the  $\phi_b - \Delta H$  line were derived to correspond to  $\phi_b^*$  correlated equations (19) and (20). In the light of the preceding discussion, only expressions for the 1 bar condition,  $K_1$  are provided and values at higher pressures in the tested range can be determined using Eqn.(17). If  $K_1$  is simply denoted as K, the expression relevant to the regimes covered by Eqn.(19) is

$$K = c_4 \left\{ \left[ \frac{1 + c_1 (c_3)^{1/2} / \rho_1^{1/2}}{1 + c_2 (c_3)^{1/2} / \rho_1^{1/2}} \right] \left[ \frac{1 + c_3 (I_h/d_h)^2}{1 + c_2 (I_h/d_h)^2} \right]^{-1} \right\} \quad (21)$$

Similarly, for the regimes covered by Eqn.(20)

$$K = k_3 \left\{ \left( G_1^{1/2} / \rho_1^{1/2} \right) \left[ \frac{k_4 + k_5 (I_h/d_h)}{1 + k_6 (I_h/d_h)} \right]^{-1} \right\} \quad (22)$$

For the C-regime of even-clusters the exponent  $\Omega$  and constants  $k_4 - k_6$  have different values for the L-(low) and H-(high) enthalpy regimes. The constants associated with Eqns. (21) and (22) are listed in Tables 3(a) and 3(b) respectively.

with the  $\phi_b$ -axis (at  $\Delta H = 0$ , see Fig.4.). Following the same procedure as before  $\phi_b^*$  was correlated in terms of the parameters in Eqn.(6). Since  $\phi_b^*$  is an arbitrary quantity which has no physical significant it was then expressed in terms of  $\phi_b$ , the extrapolated value for L-regime at  $\Delta H = 0$  and the coefficient  $\beta$  defined as

$$\beta = \phi_b^* / \phi_b^0 \quad (23)$$

Thus, from the variations of  $\phi_b^*$  and  $\phi_b^0$  in terms of the dimensionless numbers the parameter  $\beta$  simplifies to the form

$$\beta = 1.075 \left( \frac{G_1^{1/2} P_1}{\rho_1^{1/2} P_1} \right)^{0.066} \left( \frac{1 + 0.0036 (I_h/d_h)}{1 + 0.0156 (I_h/d_h)} \right) \quad (24)$$

### (iii) Burnout - Exit Quantity ( $\phi_b - \chi_{ex}$ ) Relationship

In the literature one finds burnout fluxes expressed in terms of exit quantity,  $\chi_{ex}$ . If we define

$$Q_b = \phi_b P_b I_b, \quad m = GA_1 \quad \text{and} \quad d_b = 4A_1/P_b$$

then  $\Delta H_b$  can be replaced by  $\chi_{ex}$  in Eqn. (1):

$$\frac{\Delta H_b}{H_{fg}} = \frac{4\phi_b}{GH_{fg}d_b} \frac{I_b}{d_b} - \chi_{ex} \quad (25)$$

Table 3(a) Constants of Eqn.(21)

Geometry	Flow Regime	c <sub>1</sub>	c <sub>2</sub>	c <sub>3</sub>	c <sub>4</sub> x 10 <sup>3</sup>
Even	A	8.17	2.266	8.630	6.0
	B		1.462	1.207	13.6
Odd	A	8.17	0.992	2.270	36.0
	B		1.198	0.104	4.0

Table 3(b) Constants and Exponents of Eqn.(22)

Geometry	Flow Regime	Endalpy	k <sub>1</sub>	k <sub>2</sub>	k <sub>3</sub> x 10 <sup>3</sup>	k <sub>4</sub> x 10 <sup>3</sup>	Q
Even	C	L	9.732	0.965	3.45	-1.0	-0.046
Odd	B	H	8.17	0.906	14.10	-1.0	-0.112
		*		1.204			7.0

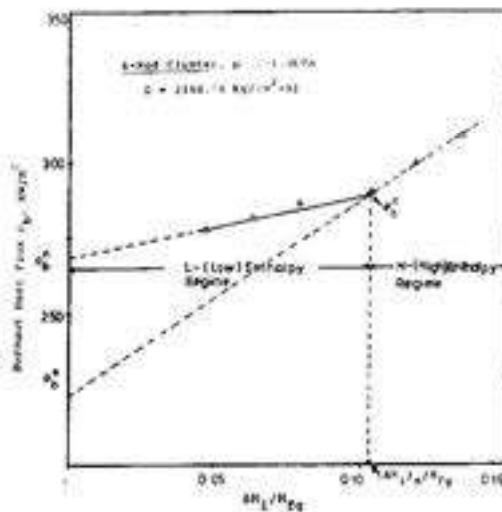


Fig.4: Positions of Burnout Heat Fluxes ( $\phi_b^*$ ,  $\phi_b^{**}$ ,  $\phi_b^{**}$ ) of 6-Rod Cluster, C-Regimes.

Multiplying the first term on the RHS by  $[(\gamma^* p) / (\rho^* p_1)] [(\gamma^* p) / (\rho^* p_1)]$  yields

$$\frac{\Delta H}{H_0} = \frac{\phi_b \gamma^{1/2}}{K_{eff} p_1^{1/2}} \frac{p/p_1}{(G \gamma^{1/2} p / D_1^{1/2} p_1)} \frac{1}{\sigma_b} - \chi_{ax} \quad (26)$$

Now the term  $\Delta H/H_0$  in Eqns.(5) and (9) can be eliminated using expression (26).  $\phi_b$  is then made subject of the equations both sides of the equations

multiplied by  $\gamma^* / (H_0 p_1^* \rho_1^*)$ . The equation corresponding to the linear  $\phi_b - \Delta H$  relationship of Eqn. (5) becomes

$$\frac{\phi_b \gamma^{1/2}}{K_{eff} p_1^{1/2}} = \frac{K_{eff} \chi_{ax} - 1}{\left[ \frac{1}{\sigma_b} \frac{p}{K_{eff} p_1} \frac{K_{eff}}{(G \gamma^{1/2} p / D_1^{1/2} p_1)} \right] - \left[ \frac{1}{\sigma_b} \frac{\phi_b \gamma^{1/2}}{K_{eff} p_1^{1/2}} \right]} \quad (27)$$

The identical relation corresponding to Eqn.(9) is given by

$$\frac{\phi_b \gamma^{1/2}}{K_{eff} p_1^{1/2}} = \frac{K_{eff} \chi_{ax} - 1}{\left[ \frac{1}{\sigma_b} \frac{p}{K_{eff} p_1} \frac{K_{eff}}{(G \gamma^{1/2} p / D_1^{1/2} p_1)} \right] - \left[ \frac{1}{\sigma_b} \frac{\phi_b \gamma^{1/2}}{K_{eff} p_1^{1/2}} \right]} \quad (28)$$

It is possible to relate the  $\phi_b - \chi_{ax}$  equations in terms of the parameters  $G \gamma^* p / \rho_1^* p_1$ ,  $p_1 / \rho_1$ , and  $l/d$ , only by substituting the relevant  $\phi_b$  expressions for different flow regimes in Eqns.(27) and (28). The relationship corresponding to Eqn.(19) then becomes:

$$\frac{\phi_b \gamma^{1/2}}{K_{fg} \rho_f^{1/2}} = c_1 \left[ 1 + c_2 \frac{G \gamma^{1/2} \mu}{\rho_f^{1/2} P_1} \right] \times \left[ \frac{K_{ex} - 1}{c_1 \left[ c_2 + \frac{1/2 G \gamma^{1/2} \mu}{\rho_f^{1/2} P_1} \right] \frac{L_h}{P_1} \frac{K_{ex}}{d_h} - \left[ \frac{c_2 L_h}{d_h} + 1 \right] \left[ \frac{\rho_f}{\rho_v} \right]^{-1}} \right] \quad (29)$$

Similarly, the relationship for the flow regimes satisfying Eqn.(20) is

$$\frac{\phi_b \gamma^{1/2}}{K_{fg} \rho_f^{1/2}} = K_L \left[ \frac{G \gamma^{1/2} \mu}{\rho_f^{1/2} P_1} \right]^{\beta} \left[ \frac{K_{ex} - 1}{K_L \left[ \frac{G \gamma^{1/2} \mu}{\rho_f^{1/2} P_1} \right]^{\beta-1} \frac{L_h}{P_1} \frac{K_{ex}}{d_h} - \left[ K_L \frac{L_h}{d_h} + 1 \right] \left[ \frac{\rho_f}{\rho_v} \right]^{-1}} \right] \quad (30)$$

In the H-(high) enthalpy regime of C-flow regime of even numbered rod clusters, substitution of Eqn.(20) in Eqn.(28) followed by rearrangement gives the equation:

$$\frac{\phi_b \gamma^{1/2}}{K_{fg} \rho_f^{1/2}} = K_H \left[ \frac{G \gamma^{1/2} \mu}{\rho_f^{1/2} P_1} \right]^{\beta} \left[ \frac{K_{ex} - 1}{K_H \left[ \frac{G \gamma^{1/2} \mu}{\rho_f^{1/2} P_1} \right]^{\beta-1} \frac{L_h}{P_1} \frac{K_{ex}}{d_h} - \left[ K_H \frac{L_h}{d_h} + 1 \right] \left[ \frac{\rho_f}{\rho_v} \right]^{-1}} \right] \quad (31)$$

The ranges of  $\chi_{ex}$  for the different flow regimes are found from Eqn.(25) using the corresponding values of  $\Delta H_f/H_{fg}$ . Eqn.(31) should only be used for exit qualities below the point of break in the  $\phi_b$ - $\chi_{ex}$  line.

(iv) Criterion for a break in  $\phi_b$ - $\chi_{ex}$  relationship

It has been mentioned that for even-numbered peripheral rods in the C-regime (high mass velocity) the relationship between  $\phi_b$  and  $\Delta H_f/H_{fg}$  or  $\chi_{ex}$  is represented by two straight lines with different slopes  $K_L$  (low enthalpy) and  $K_H$  (high enthalpy). The quantity  $\chi_{ex}$  where these two lines intersect can be found from Eqns. (27) and (28). We denote the slope  $K_L$  and the burnout flux  $\phi_{b,L}$  in Eqn. (27) and corresponding  $K_H$  and  $\phi_{b,H}$  in Eqn.(28). For the intersect  $\phi_{b,L} = \phi_{b,H}$  yielding:

$$\chi_{ex}^{br} = \frac{\xi (K_H - K_L) + \beta - 1}{\beta K_H - K_L} \quad (32)$$

where

$$\xi = 4\beta \left( \frac{\phi_b \gamma^{1/2}}{K_{fg} \rho_f^{1/2}} \right) \left( \frac{P_1}{P_2} \right) \left( \frac{L_h}{d_h} \right) \left( \frac{G \gamma^{1/2} \mu}{\rho_f^{1/2} P_1} \right)$$

Substituting for  $\phi_b \gamma^{1/2} / \rho_f^{1/2} H_{fg}$  in the expression of Eqn. (20) which satisfies  $\phi_b$  data in the C-regime of even-numbered clusters yields the relationship:

$$\chi_{ex}^{br} = \frac{K_H \left[ \left( \frac{G \gamma^{1/2} \mu}{\rho_f^{1/2} P_1} \right)^{\beta-1} \left( \frac{P_1}{P_2} \right)^{\beta} \left( \frac{L_h / d_h}{1 + K_L (L_h / d_h)} \right) \left( \frac{P_1}{P_2} \right) \right]}{K_H - K_L} \left[ K_L - K_L \right] + \beta - 1 \quad (33)$$

Exit quality values greater than  $\chi_{ex}^{br}$  computed from Eqn.(33) would be expected to lie in the L-region whereas smaller ones are associated with H-regime (high subcooling on inlet and hence low quality at exit)

(v) Boundaries for Flow Regions

For the correct selection of the set of equations predicting burnout in a given flow regime the boundaries of this regime must be specified. It is likely that transition regimes exist which lie between the three principal regions presented in the studies of Katto [4] and Dukler [5] and in this work. However, if these transition regimes are neglected then the boundaries between adjacent flow regimes can be obtained by equating the  $\phi_b \gamma^{1/2} / \rho_f^{1/2} H_{fg}$  expressions (19) and (20) relevant to flow regimes A and B and regimes B and C respectively. By following this method we obtain for

(a) Even-numbered Rod Clusters

The boundary between regimes A and B is determined by solving the equation

$$L_h / d_h = (\Gamma - 1) / \left[ (c_2)_B - \Gamma (c_2)_A \right]^{3/4}$$

where

$$\Gamma = \frac{(c_1)_B \left[ 1 + (c_2)_B (G \gamma^{1/2} \mu / \rho_f^{1/2} P_1) \right] \left( \frac{P_1}{P_2} \right)^{1-\beta}}{(c_1)_A \left[ 1 + (c_2)_A (G \gamma^{1/2} \mu / \rho_f^{1/2} P_1) \right] \left( \frac{P_1}{P_2} \right)^{1-\beta}} \quad (35)$$

The boundary between regimes B and C is determined from

$$L_h / d_h = (\Psi - 1) / \left[ (\kappa_2)_C - \Psi (\kappa_2)_B \right] \quad (36)$$

where

$$\Psi = \frac{(k_1)C}{(c_1)_B} \left( \frac{(G\gamma^{1/2}p)^{v_c}}{\rho_l^{1/2} \rho_1} \right) \left( \frac{\rho_l}{\rho_v} \right)^{v_c - v_A} \quad (37)$$

(b) Odd-numbered Rod Clusters

The boundary between regimes A and B is obtained from

$$l_w/d_h = (v-1)/[(k_2)_B - v(c_2)_A] \quad (38)$$

where

$$v = \frac{(k_1)B}{(c_1)_A} \left( \frac{(G\gamma^{1/2}p)^{v_A}}{\rho_l^{1/2} \rho_1} \right) \left( \frac{\rho_l}{\rho_v} \right)^{v_A - v_A} \quad (39)$$

Finally for the boundary between B and C flow regimes, the equation that is valid is of the form

$$l_w/d_h = (\Sigma - 1)/[(c_3)_C - \Sigma(k_2)_B] \quad (40)$$

where

$$\Sigma = \frac{(k_1)C}{(c_1)_B} \left( \frac{1 + (c_1)_C \left( \frac{G\gamma^{1/2}p}{\rho_l^{1/2} \rho_1} \right)}{\left( \frac{G\gamma^{1/2}p}{\rho_l^{1/2} \rho_1} \right)^{v_B}} \right) \left( \frac{\rho_l}{\rho_v} \right)^{v_C - v_B} \quad (41)$$

The subscripts A, B and C in all expressions stand for the flow regimes.

The solution of Eqs. (34 - 41) for  $G\gamma^{1/2}p/\rho_l^{1/2}\rho_1$  for Freon-113 at 1 bar are shown in Fig.5 for even-geometry and in Fig.6 for the odd configuration as vertical lines.

DISCUSSION AND CONCLUSION

The equations have been checked against experimental results obtained using the even- and odd-numbered rod clusters in the different flow regimes in Freon-113. On the whole, satisfactory agreement is found between predicted and experimental results. For the clusters of even geometry; the maximum RMS deviation of the experimental values for the A-regime is  $\pm 3.8\%$  and the standard deviation  $\pm 77\%$ . Considering the clusters of odd arrangement, the agreement is even better with a

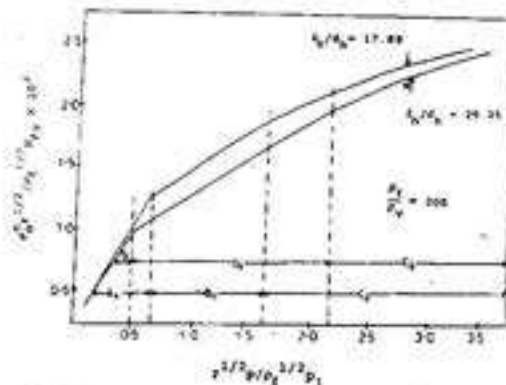


Fig.5: Variation of  $\phi_b \gamma^{1/2} / \rho_l^{1/2} H_{fg}$  with  $G\gamma^{1/2}p/\rho_l^{1/2}\rho_1$  in Flow Regimes of 6-Rod and 4-Rod Clusters (Even).

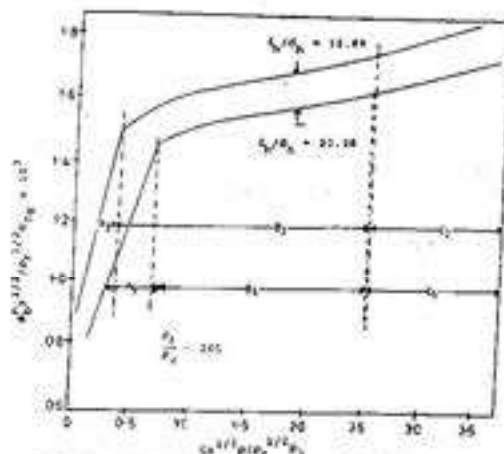


Fig.6: Variation of  $\phi_b \gamma^{1/2} / \rho_l^{1/2} H_{fg}$  with  $G\gamma^{1/2}p/\rho_l^{1/2}\rho_1$  in Flow Regimes of 5-Rod and 3-Rod Clusters (Odd).

maximum RMS of 2.38% and standard deviation of  $\pm 2.13\%$ . It can be seen that the deviations for each geometry (even or odd) are quite small and this implies that burnout heat flux are well predicted by a particular set of equations for a certain geometrical pattern of rod-cluster.

No equations were found in the literature which could correspond to the geometrical characteristics of the tested rod clusters at the low pressures used in this study. However, for the characteristics of the present 5-rod and 6-rod clusters, Macbeth [13] derived equation for boiling water at 69 bars ( $\rho_l/\rho_v = 20.6$ ) and Tong's correlation W-3 [14] for water at 138 bars ( $\rho_l/\rho_v = 7.2$ ) ought to be suitable for B- and C- flow regimes, albeit at high pressures. In

order to achieve a meaningful comparison, the scaling factors based on Eqn.(5) were used to compute the burnout fluxes at high pressures and then scaled from high pressure to low pressure. The plot of  $\phi_b$  vs.  $p$  for water system shown in Collier's [6] book was used to extrapolate the curve for 69 bars and 138 bars to 8.44 bars (corresponding to 1 bar of Freon-113) to obtain the pressure scaling factors of 1.57 and 3.40 respectively.

The burnout heat fluxes obtained in this manner were compared for the even-numbered clusters in Fig.7 and in Fig.8 for odd-numbered cluster with predictions using the equations. The comparison shows reasonable agreement with the correlations in the B-regime and in the low exit quality region of the C-regime as far as the absolute values of  $\phi_b$  are concerned. However, at high flow rates and higher exit qualities, the present results are substantially higher than those predicted by both correlations. This is obviously due to the break and change in slope which is not reflected in the water-correlations developed for high pressure systems. On the other hand, the comparison in Fig.8 shows the anomalous behaviour of the odd-numbered clusters. Since rod clusters in nuclear reactors are normally of the even type therefore will have provided the data on which Macbeth's correlation is based, one would not expect it to predict burnout values for the anomalous clusters correctly.

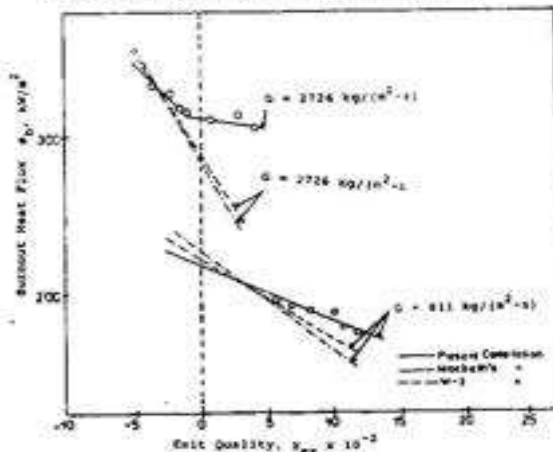


Fig.7: Comparison of Present Correlation with Macbeth's [13] and W-3 [14] for 6-Rod Cluster (Even).

Comparing the equations with Bernath's correlation [1] derived for annuli and Bowring's [15] equation for uniformly heated tubes indicate large deviations in mass velocity regime, as shown in Fig.9. Quali-

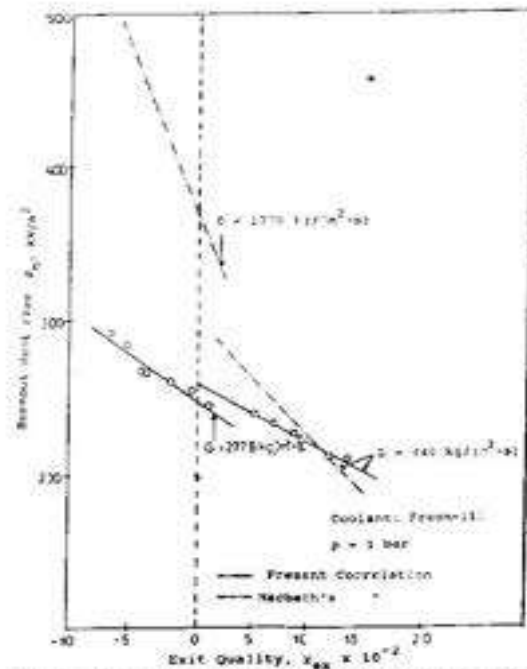


Fig.8: Comparison of Present Correlation with Macbeth's [13] for 5-Rod Cluster (Odd).

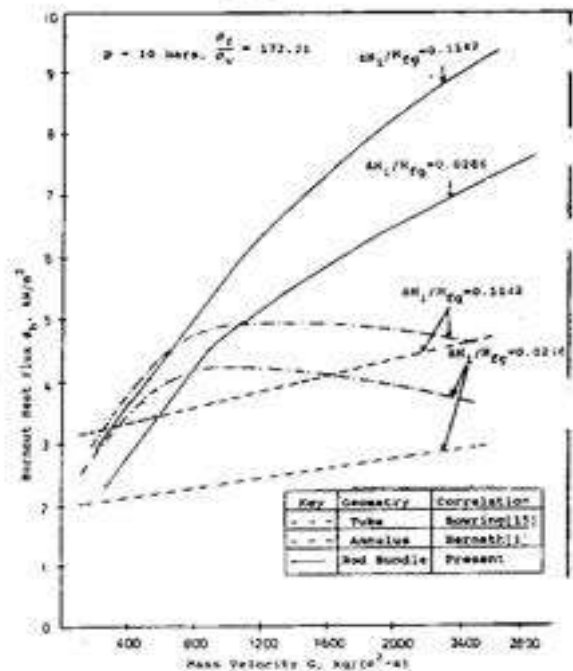


Fig.9: Comparison of Predicted Water Burnout Results Using Present Equation with Correlations for Simpler Geometries (Tubes and Annuli).

tatively, this observation is consistent with the result that burnout data in circular tubes, annuli and rod bundles do not follow the same trend. However, the trends followed by low pressure burnout data in the above mentioned geometries could be confirmed by experiments under low pressure conditions.

The correlating equations were developed in terms of the dimensionless properties suggested in Eqn.(6) for a modelling fluid, Freon-113. In order to assess their more general validity the present correlation must be adopted for other coolants. The original expression  $G\gamma^0/\rho_1^0$  proposed by Barnett was modified to  $G\gamma^0$

$p/\rho_1^0 p_1$ . It is hoped that the equations can be used to predict the burnout data for any other saturated fluid in the density ratio,  $\rho_1/\rho_v = 205 - 125$  investigated in this study. Hence, a reference pressure  $P_{ref}$  is chosen at which the density ratio is the same as for Freon-113 at 1 bar, i.e.  $\rho_1/\rho_v = 205$ . This means that the Eqns.(19) and (20) would be substituted by the fluid properties of the coolant.

In order to obtain this more general form the pressure corresponding to  $\rho_1/\rho_v$  of 205 is denoted as  $P_{ref}$  so that the term  $G\gamma^0 p/\rho_1^0 p_1$  becomes  $G\gamma^0 p/P_{ref}$ . Now, we could expect that if in different liquids the terms  $h_0/d_w$ ,  $\rho_1/\rho_v$  and  $G\gamma^0 p/P_{ref}$  are equal then the term  $\phi_b \gamma^0/\rho_1^0 H_{fg}$  will be equal too. The parameter K can be determined for any pressure (within the  $\rho_1/\rho_v$  range of 205 - 125 in this study) using Eqn.(17) with  $K_1$  becoming  $K_{ref}$  and  $(H_{fg})_1$  as  $(H_{fg})_{ref}$ .  $K_{ref}$  must be evaluated using fluid properties at  $P_{ref}$  ( $\rho_1/\rho_v = 205$ ) and  $\gamma = d(\rho_1/\rho_v)/dP_{ref}$ .

The fluid properties of  $H_2O$ , Freon-22 and  $NH_3$  were used for predicting  $\phi_b \gamma^0/\rho_1^0 H_{fg}$  values from the derived set of equations for  $\rho_1/\rho_v = 205$  and plotted in Fig.10 and for  $\rho_1/\rho_v = 133$  in Fig.11. All calculated values fall on one line together with the Freon-113 data, but for a conclusive proof that equations are universally applicable, experimental data for different fluids are necessary.

In summary, modelling of the burnout heat flux has been demonstrated for even- and odd- numbered peripheral rods. The deviations for each geometry (even or odd) are quite small and this implies that burnout heat fluxes are well predicted by a particular set of equations for a certain geometrical pattern of a rod-cluster.

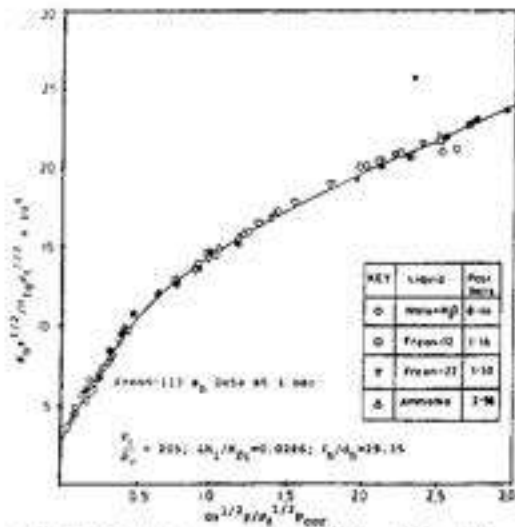


Fig.10: Variation of  $\phi_b \gamma^{1/2}/H_{fg} \rho_1^{1/2}$  with  $G \rho_1^{1/2} p/\rho_1^0 P_{ref}$  for  $\rho_1/\rho_v = 205$ .

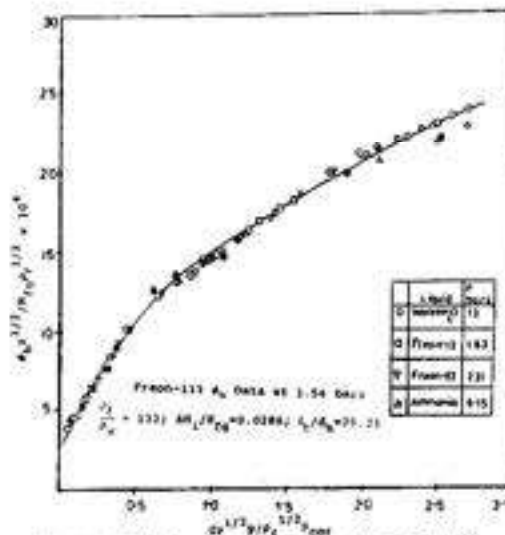


Fig.11: Variation of  $\phi_b \gamma^{1/2}/H_{fg}$  with  $G \rho_1^{1/2} p/\rho_1^0 P_{ref}$  for  $\rho_1/\rho_v = 133$ .

## 5 NOTATION

$A_f$  flow area ( $m^2$ )

$c_1, c_2$  constants in Eqns. (19) & (21)

$c_{p1}$  specific heat at constant pressure, ( $kJ/kg^\circ C$ )

$d_h$	heated hydraulic diameter = $4 \times$ flow area/heated perimeter(m).
$G$	mass velocity ( $\text{kg/m}^2\text{-s}$ )
$H_{fg}$	enthalpy of vaporization, ( $\text{kJ/kg}$ )
$\Delta H_l$	enthalpy of subcooling ( $\text{kJ/kg}$ )
$k_l$	thermal conductivity of liquid ( $\text{kW/m}^2\text{C}$ )
$k_1 - k_2$	Constants in Eqns.(17) and (19)
$l_h$	heated length (m)
$m$	mass flow rate ( $\text{kg/s}$ )
$P_h$	heated perimeter (m)
$p$	absolute pressure ( $\text{N/m}^2$ )
$Q_b$	burnout power ( $\text{KW/m}^2$ )

#### Greek Symbols

$\beta$	parameter, Eqn.(24)
$\gamma$	$d(\rho_l \rho_v) / d p_{\infty}$ ( $\text{m}^2/\text{N}$ )
$\rho_l$	density of liquid phase ( $\text{kg/m}^3$ )
$\rho_v$	density of vapour phase ( $\text{kg/m}^3$ )
$e$	exponent, Eqn.(19)
$\sigma$	exponent, Eqn.(20)
$\nu$	exponent, Eqn.(20)
$\phi_b$	burnout heat flux ( $\text{kW/m}^2$ )

Note:

$$\text{error} = \frac{\phi_b \text{ measured} - \phi_b \text{ predicted}}{\phi_b \text{ measured}}$$

$$\text{RMS error} = \frac{\sqrt{\sum(\text{error})^2}}{N}$$

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